

FORM PTO 1390  
(REV 5-93)

US DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE


ATTORNEY DOCKET NUMBER  
2001\_0698ATRANSMITTAL LETTER TO THE UNITED STATES  
DESIGNATED/ELECTED OFFICE (DO/EO/US)  
CONCERNING A FILING UNDER 35 U.S.C. §371U.S. APPLICATION NO.  
(if known, PCT OR 1)  
NEW 097857415International Application No.  
PCT/NO99/00091International Filing Date  
March 17, 1999Priority Date Claimed  
December 4, 1998Title of Invention  
METHOD FOR RECOVERING CO<sub>2</sub>Applicant(s) For DO/EO/US  
Knut Ingvar Åsen, Kjersti Wilhelmsen, and Tor Bruun

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. ☒ This is a **FIRST** submission of items concerning a filing under 35 U.S.C. §371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. §371.
3. ☒ This express request to begin national examination procedures (35 U.S.C. §371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. §371(b) and PCT Articles 22 and 39(1).
4. ☒ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5. ☒ A copy of the International Application as filed (35 U.S.C. §371(c)(2)) (in English)
  - a. ☐ is transmitted herewith (required only if not transmitted by the International Bureau).
  - b. ☒ has been transmitted by the International Bureau.
  - c. ☐ is not required, as the application was filed in the United States Receiving Office (RO/US)
6. ☐ A translation of the International Application into English (35 U.S.C. §371(c)(2)).
7. ☒ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. §371(c)(3)).
  - a. ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
  - b. ☐ have been transmitted by the International Bureau.
  - c. ☐ have not been made; however, the time limit for making such amendments has NOT expired.
  - d. ☒ have not been made and will not be made.
8. ☐ A translation of the amendments to the claims under PCT Article 19.
9. ☒ An oath or declaration of the inventor(s) (35 U.S.C. §371(c)(4)). (Unexecuted)
10. ☐ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. §371(c)(5)).

Items 11. to 14. below concern other document(s) or information included:

11. ☒ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
12. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
13. ☒ A **FIRST** preliminary amendment.  
☐ A **SECOND** or **SUBSEQUENT** preliminary amendment.
14. ☒ Other items or information: (a) PCT Request; (b) Forms PCT/IB/304 and 308; (c) International Search Report; (d) International Preliminary Examination Report; and (e) Published International Application (WO 00/33942) including drawings (A4 paper) for Figs. 1 and 2.

U.S. APPLICATION NO. <b>09/857415</b> NEW		INTERNATIONAL APPLICATION NO. PCT/NO99/00091		ATTORNEY'S DOCKET NO. 2001_0698A					
15. [X] The following fees are submitted  <b>BASIC NATIONAL FEE (37 CFR 1.492(a)(1)-(5)):</b> Neither international preliminary examination fee nor international search fee paid to USPTO and International Search Report not prepared by the EPO or JPO ..... \$1000.00 International Search Report has been prepared by the EPO or JPO ..... \$ 860.00 International preliminary examination fee not paid to USPTO but international search paid to USPTO ..... \$ 710.00 International preliminary examination fee paid to USPTO but claims did not satisfy provisions of PCT Article 33(1)-(4) ..... \$ 690.00 International preliminary examination fee paid to USPTO and all claims satisfied provisions of PCT Article 33(1)-(4) ..... \$ 100.00  <b>ENTER APPROPRIATE BASIC FEE AMOUNT =</b>				<table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:50%;">CALCULATIONS</th> <th style="width:50%;">PTO USE ONLY</th> </tr> <tr> <td style="height: 100px;"></td> <td></td> </tr> </table>		CALCULATIONS	PTO USE ONLY		
CALCULATIONS	PTO USE ONLY								
Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(e)).				\$					
Claims	Number Filed	Number Extra	Rate						
Total Claims	11 -20 =	0	X \$18.00	\$					
Independent Claims	1 - 3 =	0	X \$80.00	\$					
Multiple dependent claim(s) (if applicable)			+ \$270.00	\$					
<b>TOTAL OF ABOVE CALCULATIONS =</b>				\$1000.00					
<input type="checkbox"/> Small Entity Status is hereby asserted. Above fees are reduced by 1/2.				\$					
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<b>TOTAL NATIONAL FEE =</b>				\$1000.00					
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40 per property +				\$					
<b>TOTAL FEES ENCLOSED =</b>				\$1000.00					
				Amount to be refunded	\$				
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a. [X] A check in the amount of \$1000.00 to cover the above fees is enclosed. A duplicate copy of this form is enclosed. b. <input type="checkbox"/> Please charge my Deposit Account No. 23-0975 in the amount of \$_____ to cover the above fees. A duplicate copy of this sheet is enclosed. c. <input type="checkbox"/> The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. 23-0975.									
<b>NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or          (b)) must be filed and granted to restore the application to pending status.</b>									
19. CORRESPONDENCE ADDRESS  <div style="text-align: center;">   <b>000513</b>          PATENT TRADEMARK OFFICE       </div>			By: <u>Michael R. Davis</u> Michael R. Davis, Registration No. 25,134  WENDEROTH, LIND & PONACK, L.L.P. 2033 "K" Street, N.W., Suite 800 Washington, D.C. 20006-1021 Phone: (202) 721-8200 Fax: (202) 721-8250  June 4, 2001						

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JC03 Rec'd PCT/PTC 04 JUN 2001

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re application of	:	
Knut Ingvar ÅSEN et al.	:	<b>Attn: BOX PCT</b>
Serial No. NEW	:	<b>Docket No. 2001_0698A</b>
Filed June 4, 2001	:	

**METHOD FOR RECOVERING CO<sub>2</sub>**  
**[Corresponding to PCT/NO99/00091**  
**Filed March 17, 1999]**

**PRELIMINARY AMENDMENT**

Assistant Commissioner for Patents,  
Washington, DC 20231

Sir:

Please amend the above-identified application as follows:

## IN THE SPECIFICATION

Page 1, after the title of the invention, please insert:

--This application is a 371 application of PCT/NO99/00091 filed March 17, 1999.--

## REMARKS

The specification has been amended to insert a cross reference to the International Application on which the present application is based.

Respectfully submitted,

Knut Ingvar ASEN et al.

By

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Registration No. 25,134  
Attorney for Applicants

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09/ 857415

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Method for recovering CO<sub>2</sub>

The present invention relates to a method for recovering substantially all CO<sub>2</sub> generated in a combustion process which includes an application of a mixed conducting membrane. Furthermore, the present invention relates to use of this method.

Due to the environmental aspects of CO<sub>2</sub>, the possibilities for reducing the emissions of this compound to the atmosphere from combustion processes has been widely discussed.

Conventional combustion processes, used for carbon containing fuels and where the oxygen source is air, having carbon dioxide concentrations of 3-15% in the combustion products, hereinafter called exhaust gas, dependent on the fuel and the applied combustion- and heat recovery process. The reason the concentration is this low is because air is made up of about 78% by volume of nitrogen.

Thus, a reduction in the emission of carbon dioxide to the atmosphere makes it necessary to either separate the carbon dioxide from the exhaust gas, or raise the concentration to levels suitable for use in different chemical processes or for injection and deposition in e.g. a geological formation for long term deposition or for enhanced recovery of oil.

CO<sub>2</sub> can be removed from cooled exhaust gas, normally discharged off at near atmospheric pressure, by means of several separation processes e.g. chemical

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active separation processes, physical absorption processes, adsorption by molecular sieves, membrane separation and cryogenic techniques. Chemical absorption for instance by means of alkanole amines is e.g. considered as the most practical and economical method to separate CO<sub>2</sub> from exhaust gas. The separation processes, however, require heavy and voluminous equipment and will consume a substantial amount of heat or power. Applied in a power generation process, this process will reduce the power output with around 10% or more.

An increase of the concentration of CO<sub>2</sub> in the exhaust gas to levels suitable for use in different chemical processes or for injection and deposition e.g. in a geological formation for long term deposition or for enhanced recovery of oil from an oil reservoir is possible by burning fuel in pure oxygen instead of air.

Commercial air separation methods (e.g. cryogenic separation or pressure swing absorption (PSA)) used to produce pure oxygen require 250 to 300 KWh/ton oxygen produced. Supplying oxygen e.g. to a gas turbine by this methods will decrease the net power output of the gas turbine cycle by at least 20%. The cost of producing oxygen in a cryogenic unit will increase the cost of electric power substantially and may constitute as much as 50% of the cost of the electric power.

However, a less energy demanding method than the separation methods mentioned above is known from European patent application 0658 367- A2 which describes an application of a mixed conducting membrane which is integrated with a gas turbine system by heating air in a gas turbine combustor and further by selective permeation of oxygen through the membrane. Pure oxygen near atmospheric pressure or below and at high temperature is recovered from the permeate side of the conducting membrane. An oxygen partial pressure difference causes oxygen to be transported through the membrane by reduction of oxygen on the high oxygen partial pressure side (retentate side) and oxidation of oxygen ions to oxygen gas on the low oxygen partial pressure side (the permeate side). In the bulk of the membrane oxygen ions are transported by a diffusion process. Simultaneously the electrons flow from the permeate side back to the feed side of the membrane.

Application of a sweep gas in combination with a mixed conducting membrane to lower the oxygen partial pressure to increase the degree of oxygen removal or oxygen recovery is known from the US patent 5562754. In this patent a method for combined production of oxygen and power is disclosed by heating air in a gas turbine combustor and by selective permeation of oxygen through the membrane. In order to improve the efficiency of gas separation by the membrane, the permeate side of the membrane is swept by e.g. steam supplied for instance from the heat recovery section of the power plant. The sweep gas is heated in a separate high temperature heat exchanger. The application of sweep gas will reduce the partial pressure of oxygen on the permeate side of the membrane and thereby increase the flux of oxygen through the membrane.

However, this requires a certain amount of sweep gas and therefore a certain energy amount to generate this sweep gas. This will therefore decrease the net power output of the power generating process.

Application of a sweep gas in combination with a mixed conducting membrane is also known from Norwegian patent application NO-A-972632 (published 07.12.98). This patent describes a power and heat generating process where a fuel is combusted with an oxidant, which is an  $O_2/CO_2/H_2O$ -containing gaseous mixture, which is supplied from a mixed conducting membrane. The oxygen is picked up from the permeate side of the mixed conducting membrane by means of a sweep gas. The sweep gas is the product or part of the product from at least one combustion process upstream the membrane. In this patent application the sweep gas, or part of the sweep gas, containing a mixture of mainly  $CO_2$  and  $H_2O$ , also act as the working fluid in a gas turbine cycle. The amount of sweep gas is related to the amount of working fluid required in the gas turbine cycle i.e. to control the temperature in the gas turbine combustor. Working fluid is the gas (oxidant and fuel) transported through the gas turbine system. Air fed to the retentate side of this membrane is heated by combusting a fuel in the air stream in a burner.

To obtain a sufficient high flux of oxygen through the membrane a rather high temperature is required (600 - 1500 °C). On the air side of the membrane this may

be accomplished by combusting a fuel in the air stream in a burner to increase the temperature of the air fed to the membrane, for instance as disclosed in European patent application 0658 367- A2 or as described in Norwegian patent application NO-A-972632 ( published December 7, 1998). The most convenient and least expensive method is to use a carbon containing fuel, e.g. a fossil fuel.

However, by means of this method the heated air stream will contain CO<sub>2</sub> generated in the burner. The CO<sub>2</sub> concentration in the oxygen depleted air stream discharged from the retentate side of the membrane will be less than about 10% and in most cases less than 3%. If recovery of all generated CO<sub>2</sub> in a combustion process is desirable, due to environmental aspects of CO<sub>2</sub>, an oxygen depleted air stream containing low CO<sub>2</sub> -concentrations is not desirable.

Application of a staged mixed conducting membrane process is known from US patent 5,447,555 which describes a method for producing pure oxygen. In this process high purity oxygen is recovered from air by a high-temperature ion transport membrane system comprising two or more stages in which each stage operates at a different feed side to permeate side pressure ratio. Operation of the system in multiple stages at controlled pressure ratios produces oxygen at a lower specific power consumption compared with single-stage operation. Sweep gas is not used in this US patent.

The main object of this invention was to arrive at an energy efficient method to recover substantially all CO<sub>2</sub> generated in a combustion process.

The described object can be fulfilled by application of a method which include an application of a mixed conducting membrane.

Hot steam or a mixture of steam and CO<sub>2</sub> (e.g. recycled exhaust gas) is used as sweep gas to pick up oxygen on the permeate side of a mixed conducting membrane (MCM) in a first stage. The membrane is capable of separating oxygen from a hot air stream fed to the retentate side of the membrane. Sweep gas now containing oxygen is applied as oxidant in a catalytic or non catalytic combustion process where a carbon containing fuel is combusted. Heat generated in the combustion process is used to heat air fed to the retentate side of the membrane.

The hot combustion products, i.e. the exhaust gas, containing  $\text{CO}_2$ ,  $\text{H}_2\text{O}$  and a low concentration of  $\text{O}_2$  is used as sweep gas in a second MCM stage and the concentration of oxygen in the sweep gas is increased in the second membrane stage to a sufficiently high level to be used as oxidant in a second combustion stage. Heat generated in the second combustion process is also used to heat air to the MCM-process. Hot combustion products leaving the second combustion stage is used as sweep gas to pick up more oxygen in a third MCM-stage to be used as oxidant in a third combustion stage. The number of required combustion stages and MCM-stages depends on the amount of sweep gas fed to MCM-stage one and on the required pre-heating temperature of air to the retentate side of the MCM-process.

The oxygen produced in the membrane is removed between each stage by combustion with fuel in a combustor. The partially cooled  $\text{CO}_2$  containing exhaust gas with a low concentration of oxygen is used as sweep gas in the next MCM stage.

This will reduce the amount of sweep gas necessary for production of a given amount of oxygen and thus reduce the size of equipment necessary for producing sweep gas to the first MCM stage. Application of e.g. 10 stages will reduce the amount of sweep gas with about 95% compared with a single stage process and reduce the energy required to generate sweepgas in the same order of magnitude.

Air fed to the retentate side of each mixed conducting membranes is heated by heat exchanging with hot exhaust gas generated in at least one combustor.

If sweep gas is not generated during the process or used as a working fluid in a gas turbine cycle the sweep gas has to be generated in a separate process.

If sweep gas is generated in a separate process the cost of sweep gas is related to the required amount of sweep gas. The cost of sweep gas generation will be reduced if the amount of sweep gas used in the air heating process is reduced. In a one stage mixed conducting membrane process this reduced amount of sweep gas will, however, reduce the rate of oxygen transport through the membrane.

This will further increase the required membrane area and thus the membrane costs. Otherwise the sweep gas pressure has to be reduced. This will, however,



increase the pressure drop of oxygen through the membrane and thus reduce the efficiency of the heat generating process.

In the present invention each stage operates at nearly the same pressure and the staged process will not increase the membrane area requirement. Since oxygen is removed between each stage the driving forces for transport of oxygen through the membrane will increase and reduce the membrane area requirement and the costs.

The problems mentioned above concerning reduced transport of oxygen, increased costs or reduced efficiency, if the amount of sweep gas, which may be steam or a mixture of steam and/or recycled exhaust gas, is reduced, is solved by application of the staged combined mixed conducting membrane and combustion process described in the present invention.

In order to avoid excessive temperatures in the combustion process, comprising use of catalytic or non catalytic combusters, the exhaust gas which is used as sweep gas in a subsequent mixed conducting membrane stage, is cooled between the stages by heat exchanging with air to generate hot air. Furthermore the temperature in the combustor stages are controlled by varying the concentration of oxygen in the sweep gas.

In order to obtain a sufficient high flux of oxygen through the mixed conducting membranes a high air temperature is required which is achieved by the heat exchanging method described above according to the present invention. The air stream is heated in several stages in heat exchangers located between the membrane stages or is divided into several streams and each stream is heated in a heat exchanger located between two membrane stages.

Heated air generated by the method according to the present invention can be used to generate pure oxygen in a mixed conducting membrane.

Furthermore, heated air generated by the method according to the present invention can be used to generate synthesis gas consisting of one or more of the

components CO, CO<sub>2</sub>, H<sub>2</sub> and N<sub>2</sub> or for generating heat in a mixed conducting membrane reactor where the membrane reactor is capable of reacting a mixture of steam and a carbon containing fuel with oxygen permeated through the said membrane to make synthesis gas and/or heat.

Further, the method according to the present invention is used in a heat and/or power generating process.

Further, the CO<sub>2</sub>-containing exhaust gas generated by the method according to the present invention is used for enhanced oil and natural gas recovery or for injection in a geological formation or is used in a chemical process to make carbon containing products. Oxygen eventually left in the CO<sub>2</sub> containing combustion gas exit in the last combustion stage can be removed in a catalytic oxidation reactor or in a combined mixed conducting membrane and partial oxidation reactor as described in patent application NO-A-972631 (published 07.12.98).

In a further embodiment of the invention the CO<sub>2</sub> containing exhaust gas and/or the oxygen depleted air stream is depressurized in a turbine to generate power. The invention will be further explained and envisaged in the examples and corresponding figures.

Figure 1 shows a power and heat generating process according to the invention comprising a staged MCM process with inter stage combustion and heat recovery. Air is heated in several stages.

Figure 2 shows a power and heat generating process according to the invention comprising a staged MCM process with inter stage combustion and heat recovery. The air stream from the compressor is divided into several streams and each air stream is heated in a heat exchanger located between two MCM stages.

Figure 1 shows a combined power and heat generating process comprising application of a staged Mixed Conducting Membrane (MCM) and combustors where a sweep gas 1 is fed to the permeate side 2 of a first stage MCM 3 (stage

1) to pick up oxygen transported through said membrane 3. The mixture of sweep gas and oxygen is fed to a catalytic or non-catalytic burner 5 where a fuel 6 is combusted. Hot exhaust gas 7 is fed to a heat exchanger 8 where compressed air 33 is heated. Partially cooled exhaust gas 9 is used as sweep gas on the permeate side 10 of a second MCM 11 (stage 2). Oxygen containing gas 12 is mixed with a fuel 13 in a catalytic or non-catalytic burner 14 to generate a hot exhaust gas 15. Hot exhaust gas 15 with increased amount of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  is fed to heat exchanger 16 to heat compressed air 34. Partially cooled exhaust gas 17 is used as sweep gas in a next MCM stage (not shown). The number of required MCM-stages depends on the amount of sweep gas fed to the first MCM-stage. A hot exhaust gas with increased amount of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  is used as sweep gas on the permeate side of the last MCM stage 19. Oxygen containing sweep gas 20 is mixed with a fuel 21 in a catalytic or non-catalytic burner 22 to generate a hot exhaust gas 23. This  $\text{CO}_2$ -containing exhaust gas is heat exchanged with compressed air 35 and the  $\text{CO}_2$ -containing exhaust gas 24 is further depressurized in turbine generator 25 to generate power. Depressurized exhaust gas 26 is fed to heat recovery system 27 to produce steam and condensate water 30. High concentrated  $\text{CO}_2$  is recovered and fed to a  $\text{CO}_2$  injection system 29.

Air 31 at ambient conditions is fed to compressor 32. Compressed air 33 is further heated in heat exchanger 8 and 16 and further in several stages (not shown) including the last heat exchanger 36. Heated air 37 is fed to the retentate side of MCM 19 and further through several MCM stages including MCM 11 and MCM 3. Partly oxygen depleted air 46 is depressurised in turbine generator 47 to generate power or is fed to a mixed conducting membrane capable of producing pure oxygen or synthesis gas. Depressurised oxygen depleted air 48 is fed to heat recovery system 49 and the cooled gas 50 is discharged off.

Figure 2 shows a combined power and heat generating process comprising application of a staged Mixed Conducting Membrane (MCM) process where a sweep gas 1 is fed to the permeate side 2 of a first stage MCM 3 to pick up oxygen transported through said membrane 3. The mixture of sweep gas and oxygen is fed to a catalytic or non-catalytic burner 5 where a fuel 6 is combusted.

Hot exhaust gas 7 is fed to heat exchanger 8 where compressed air is heated. Partially cooled exhaust gas 9 is used as sweep gas on the permeate side 10 of a second MCM 11 (stage 2). Oxygen containing gas 12 is mixed with a fuel 13 in a catalytic or non-catalytic burner 14 to generate a hot exhaust gas 15. Hot exhaust gas 15 with increased amount of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  is fed to heat exchanger 16 to heat compressed air. Partially cooled exhaust gas 17 is used as sweep gas in a next MCM stage (not shown). The number of required MCM-stages depends on the amount of sweep gas fed to MCM-stage one. A hot exhaust gas with increased amount of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  is used as sweep gas on the permeate side of a last MCM stage 19. Oxygen containing sweep gas 20 is mixed with a fuel 21 in a catalytic or non-catalytic burner 22 to generate a hot exhaust gas 23. This  $\text{-CO}_2$ -containing exhaust gas is heat exchanged with compressed air 35 and the gas 24 is further depressurized in turbine generator 25 to generate power. Depressurized exhaust gas 26 is fed to heat recovery system 27 to produce steam and condensate water 30. High concentrated  $\text{CO}_2$  is recovered and fed to a  $\text{CO}_2$  injection system 29.

Air 31 at ambient conditions is fed to compressor 32. Compressed air 33 is further divided into several air streams equal the number of MCM stages. Compressed air stream 35 is heated in heat exchanger 36 and the hot air stream 37 is fed to the retentate side of MCM 19. Oxygen depleted air 38 is fed to mixer 45. Compressed air stream 39 is heated in heat exchanger 16 and the hot air stream 40 is fed to the retentate side of MCM 11. Oxygen depleted air 41 is fed to mixer 45. Compressed air stream 42 is heated in heat exchanger 8 and the hot air stream 43 is fed to the retentate side of MCM 3. Oxygen depleted air 44 is fed to mixer 45. The remaining air streams from separator 51 is fed to the remaining heat exchanger and MCM-stages (not shown) and the resulting hot oxygen depleted air streams is collected in mixer 45. Oxygen depleted air 46 is depressurised in turbine generator 47 to generate power or is fed to a mixed conducting membrane capable of producing pure oxygen or synthesis gas. Depressurised oxygen depleted air 48 is fed to heat recovery system 49 and the cooled gas 50 is discharged.

### Example 1

This example shows a power generating process as described in figure 1.

A hot sweep gas 1 at about 500 to 1200 °C and at elevated pressure consisting of steam or a mixture of steam and CO<sub>2</sub> or recycled exhaust gas (part of stream 28 or stream 24) is fed to the permeate side 2 of a first Mixed Conducting Membrane (MCM) 3 (stage 1) to pick up oxygen transported through said membrane 3. The mixture of sweep gas and oxygen which may contain at least 5 % oxygen is fed to a catalytic or non-catalytic burner 5 where a fuel 6 (i.e. natural gas or synthesis gas) is combusted. Hot exhaust gas 7 at about 800 to 1500 °C is fed to heat exchanger 8 where compressed air 33 is heated up to between 500 and 750 °C. Partially cooled exhaust gas 9 at 500 to 1200 °C is used as sweep gas on the permeate side 10 of a second MCM 11 (stage 2). Oxygen containing gas 12 is mixed with a fuel 13 in a catalytic or non-catalytic burner 14 to generate a hot exhaust gas 15. Hot exhaust gas 15 at 1000 to 1500 °C with increased amount of CO<sub>2</sub> and H<sub>2</sub>O is fed to heat exchanger 16 to heat compressed air 34. Partially cooled exhaust gas 17 is used as sweep gas in a next MCM stage (not shown).

The number of required MCM-stages depends on the amount of sweep gas fed to MCM-stage one. Application of 10 MCM stages will reduce the required amount of sweep gas with about 95% compared with a one stage air heating process as shown in table 1. The amount of sweep gas inlet stage one is 233 kmol/hr and the amount of sweep gas inlet stage 10 is increased to 631 kmol/hr due to the addition of a carbon containing fuel to the burners (5,15, 22 etc.) between each MCM stage and due to addition of oxygen transported through the mixed conducting membranes. The total amount of oxygen produced in all the MCM stages is about 318 kmol/hr if the concentration of oxygen outlet each burner is 3%. By applying 10% oxygen in sweep gas out of a mixed conducting membrane in a one stage process 70% of the recovered oxygen can be used in a combustion process. The amount of sweep gas required to produce 318 kmol/hr of oxygen will then be 4443 kmol/hr. Application of 10 stages will reduce the required amount to 233 kmol/hr i.e. 95% reduction. Table 1 also shows the inlet air temperature of each heat

exchanger (8,16,36 etc.) and the concentration of CO<sub>2</sub> and H<sub>2</sub>O in inlet sweep gas of each mixed conducting membrane stage. The CO<sub>2</sub> in the exhaust gas from the last stage may be recovered by cooling the exhaust gas stream to below 50 °C to condensate water. This will increase the concentration of CO<sub>2</sub> to above 95%. A hot exhaust gas 18 at 1000 to 1300 °C with increased amount of CO<sub>2</sub> and H<sub>2</sub>O is used as sweep gas on the permeate side of the last MCM stage 19. Oxygen containing sweep gas 20 is mixed with fuel 21 in a catalytic or non-catalytic burner 22 to generate hot exhaust gas 23. This CO<sub>2</sub>-containing exhaust gas at 1100 to 1500 °C is heat exchanged with compressed air 35 and the gas 24 is further depressurized in turbine generator 25 to near atmospheric pressure to generate power. Depressurized exhaust gas 26 is fed to heat recovery system 27 to produce steam and condensate water 30. High concentrated CO<sub>2</sub> is recovered and fed to a CO<sub>2</sub> injection system 29 where CO<sub>2</sub> is compressed and dried.

Air 31 at ambient conditions is fed to compressor 32. Compressed air 33 is further heated in heat exchanger 8 and 16 and further in several stages (not shown) including the last heat exchanger 36 up to between 800 and 1400 °C. Heated air 37 is fed to the retentate side of MCM 19 and further through several MCM stages including MCM 11 and MCM 3. Oxygen depleted air 46 is depressurised in turbine generator 47 to near atmospheric pressure to generate power or is fed to a mixed conducting membrane capable of producing pure oxygen or synthesis gas. Depressurised oxygen depleted air 48 is fed to heat recovery system 49 and the cooled nitrogen-containing gas 50 is discharged off.

Table 1

Stage nr.	Inlet Air temperature, °C	%CO <sub>2</sub> in sweep gas inlet stage	%H <sub>2</sub> O in sweep gas inlet stage	O <sub>2</sub> transported through MCM kmol/hr
1	454	0	100	26.1
2	461	3.65	93.34	20.9
3	500	6.92	90.06	23.3
4	544	9.86	87.11	25.9
5	592	12.50	84.46	28.9
6	645	14.87	82.08	32.4
7	704	17.01	79.93	36.1
8	769	18.94	77.99	39.6
9	840	20.65	76.28	44.1
10	919	22.18	74.73	49.1
Exit stage 10	1 006	23.56	73.35	

### Example 2

This example shows a power generating process as described in figure 2.

The system for generation of sweep gas is the same as described in example 1 and figure 1. But compressed air 33 is further divided into several air streams equal the number of MCM stages. Compressed air stream 35 is heated in heat exchanger 36 to between 800 and 1400 °C and the hot air stream 37 is fed to the retentate side of MCM 19. Oxygen depleted air 38 is fed to mixer 45. Compressed air stream 39 is heated in heat exchanger 16 to between 800 and 1400 °C and the hot air stream 40 is fed to the retentate side of MCM 11. Oxygen depleted air 41 is fed to mixer 45. Compressed air stream 42 is heated in heat exchanger 8 to between 800 and 1400 °C and the hot air stream 43 is fed to the retentate side of MCM 3. Oxygen depleted air 44 is fed to mixer 45. The remaining air streams from separator 51 is fed to the remaining heat exchanger and MCM-stages (not shown) and the resulting hot oxygen depleted air streams is collected in mixer 45. Oxygen depleted hot air 46 at 800 to 1400 °C is depressurised in turbine generator 47 to generate power or is fed to a mixed conducting mebrane capable of producing

pure oxygen or synthesis gas. Depressurised oxygen depleted air 48 is fed to heat recovery system 49 and the cooled nitrogen-containing gas 50 is discharged.

An alternative configuration of the process according to figure 1 and 2, comprises that the CO<sub>2</sub> containing gas stream 24 is mixed with a fuel and fed to a catalytic burner in order to remove oxygen. The amount of fuel is regulated such that the concentration of oxygen is reduced to below 50 to 100 ppm. The CO<sub>2</sub> containing exhaust gas with a low concentration of oxygen is depressurised in turbine generator 25 to generate power and heat is further recovered in 27. The CO<sub>2</sub>-containing gas after recompression and drying may be injected for enhanced oil recovery.

An alternative configuration of the process according to figure 1 and 2, comprises that the CO<sub>2</sub> containing gas stream 24 is mixed with a fuel and fed to a combined mixed conducting membrane and partial oxidation reactor as described in patent application NO-A-972631 (published 06.12.98) in order to reduce the concentration of oxygen to below 10 ppm. The CO<sub>2</sub> containing exhaust gas with a low concentration of oxygen is depressurised in turbine generator 25 to generate power and heat is further recovered in 27. The CO<sub>2</sub>-containing gas after recompression and drying may be injected for enhanced gas and oil recovery.

An alternative configuration of the process according to figure 1 and 2, comprises that the CO<sub>2</sub> containing gas stream 23 is depressurised in turbine 25 without heatexchanging with air in heat exchanger 36.

Fuel useful in the processes described in example 1 and 2 comprises natural gas, methanol, synthesis gas comprising hydrogen and carbon monoxide, refinery fuel gas containing mixed hydrocarbons or other combustible mixtures.

By the present invention the inventors has arrived at an efficient method to recover substantially all CO<sub>2</sub> generated in a combustion process.



The required amount of sweep gas may be reduced without increasing the required mixed conducting membrane area or without reducing the partial pressure of recovered oxygen. This will reduce the costs and increase the process efficiency.

The method according to the present invention can be used in several types of heat and power generating processes as Combined Cycle Power Plants, in Cogeneration power and heat plants, in Integrated Gasification and Combined Cycle power plants, in any processes comprising combustion of a fuel or for heating purposes e.g. in chemical plants or for heating air fed to mixed conducting membranes.

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## CLAIMS

1. A method for recovering substantially all carbon dioxide generated in a combustion process,  
c h a r a c t e r i s e d i n t h a t  
the method comprises the following steps:
  - a) a sweep gas is used to pick up oxygen on the permeate side of a mixed conducting membrane in a first stage which is capable of separating oxygen from a hot air stream fed to the retentate side of the membrane
  - b) the sweep gas containing oxygen is applied as oxidant in a combustor in the first stage where a carbon containing fuel is combusted
  - c) hot combustion products of step b) containing CO<sub>2</sub>, H<sub>2</sub>O and a low concentration of O<sub>2</sub> is used as sweep gas in a membrane in a second stage downstream the combustor in step b)
  - d) the concentration of oxygen in the sweep gas of step c) is increased in the membrane in the second stage ( step c) to a sufficiently high level to be used as oxidant in the combustor in the second stage
  - e) and the steps c) - d) are repeated in one or more stages.
2. A method for recovering substantially all carbon dioxide generated in a combustion process according to claim 1,  
c h a r a c t e r i s e d i n t h a t  
the combustor is a catalytic or non catalytic combustor.
3. A method for recovering substantially all carbon dioxide generated in a combustion process according to claim 1,  
c h a r a c t e r i s e d i n t h a t

the sweep gas used in step a) is hot steam or a mixture of steam and/or recycled exhaust gas from the last combustor in the sequence.

4. A method for recovering substantially all carbon dioxide generated in a combustion process according to claim 1,  
characterised in that  
the mixed conducting membrane is made from materials with both ionic and electronic conductivity.
5. A method for recovering substantially all carbon dioxide generated in a combustion process according to claim 1,  
characterised in that  
the air stream is heated by heat exchanging with hot exhaust gas generated in at least one combustor.
6. A method for recovering substantially all carbon dioxide generated in a combustion process according to claim 1,  
characterised in that  
the air stream, before being heated, is compressed and divided into several streams and each stream is heated in a heat exchanger located between two membrane stages.
7. Use of the method according to claim 1, for generating heat and power.
8. Use of the exhaust gas recovered by the method according to claim 1, for enhanced oil recovery or for injection in a geological formation.
9. Use of the exhaust gas recovered by the method according to claim 1, in a chemical process to make carbon containing products.
10. Use of heated air generated by the method according to claim 1, for generating pure oxygen in a mixed conducting membrane.

11. Use of heated air generated by the method according to claim 1, for generating synthesis gas consisting of one or more of the components CO, CO<sub>2</sub>, H<sub>2</sub> and N<sub>2</sub> or for generating heat in a mixed conducting membrane reactor where the membrane reactor is capable of reacting a mixture of steam and a carbon containing fuel with oxygen permeated through the said membrane to make synthesis gas and/or heat.

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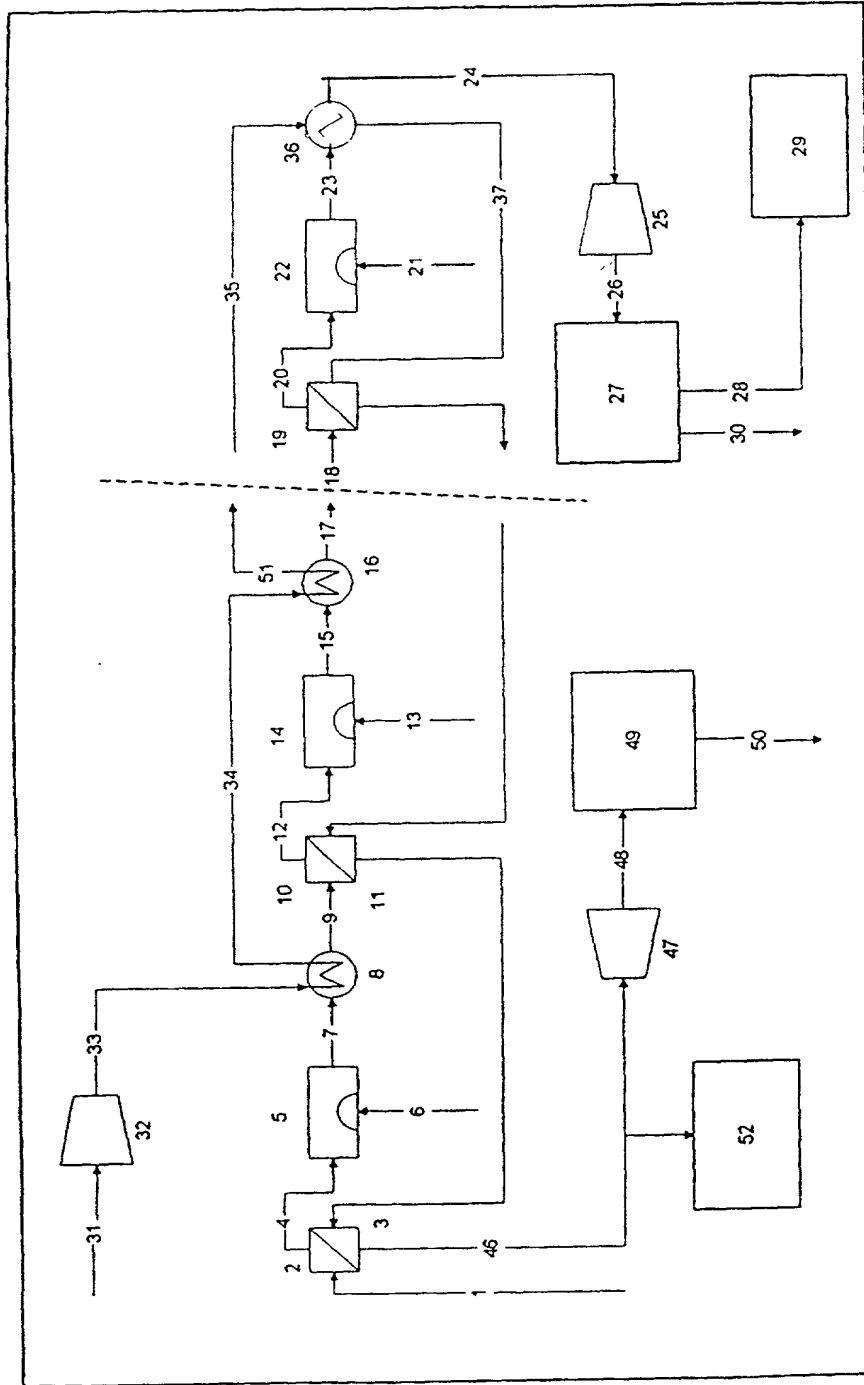
[illegible]

Figure 1

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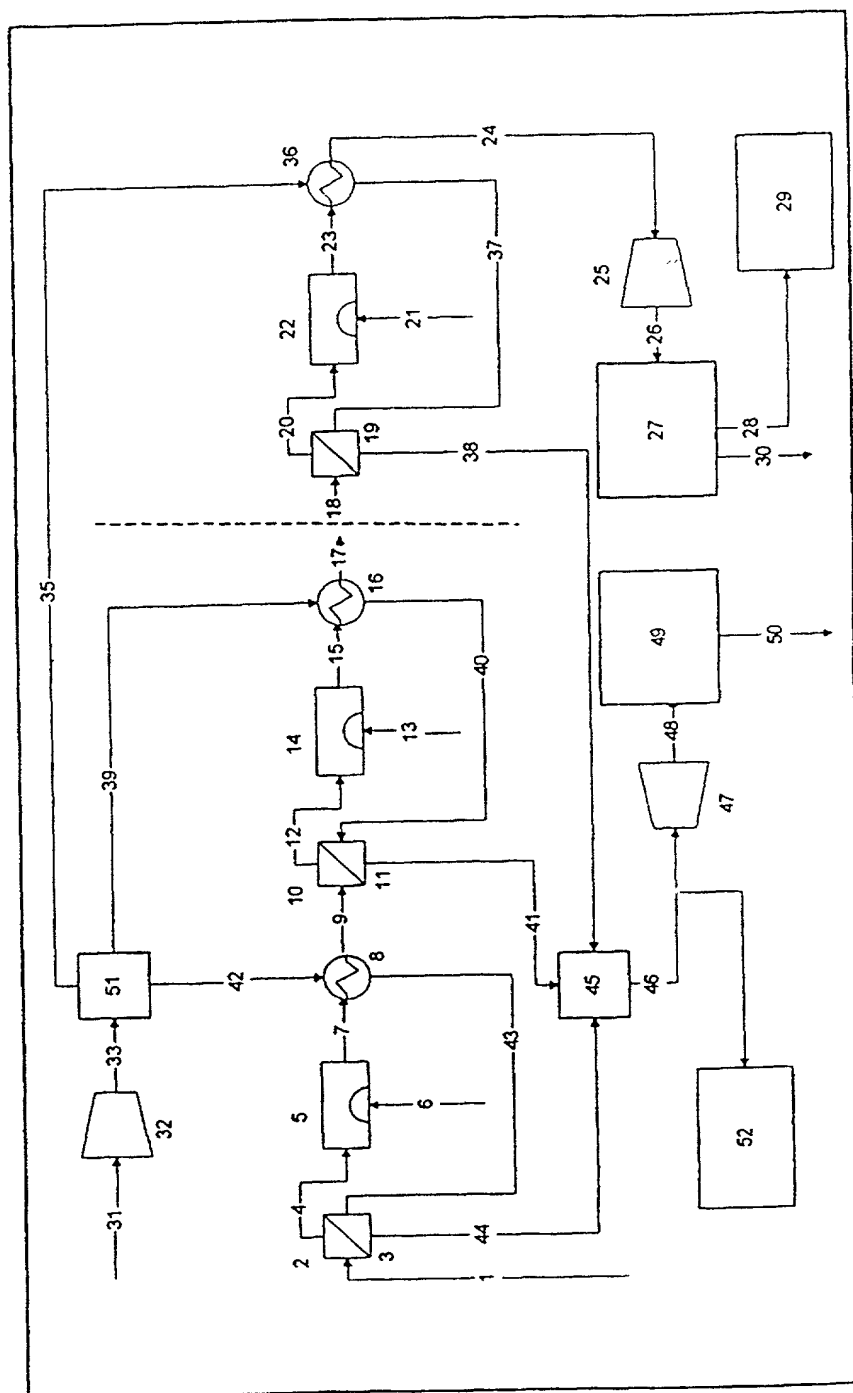


Figure 2

## DECLARATION AND POWER OF ATTORNEY FOR U.S. PATENT APPLICATION

(X) Original    () Supplemental    () Substitute    () PCT    () DESIGN

As a below named inventor, I hereby declare that: my residence, post office address and citizenship are as stated below next to my name; that I verily believe that I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural inventors are named below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

Title: METHOD FOR RECOVERING CO<sub>2</sub>

of which is described and claimed in:

() the attached specification, or

() the specification in application Serial No., filed , and with amendments through \_\_\_\_\_, or

(X) the specification in International Application No. PCT/NO99/00091, filed March 17, 1999, and as amended on \_\_\_\_\_ (if applicable).

I hereby state that I have reviewed and understand the content of the above-identified specification, including the claims, as amended by any amendment(s) referred to above.

I acknowledge my duty to disclose to the Patent and Trademark Office all information known to me to be material to patentability as defined in Title 37, Code of Federal Regulations, §1.56.

I hereby claim priority benefits under Title 35, United States Code, §119 (and §172 if this application is for a Design) of any application(s) for patent or inventor's certificate listed below and have also identified below any application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

COUNTRY	APPLICATION NO.	DATE OF FILING	PRIORITY CLAIMED
Norway	19985706	December 4, 1998	yes

I hereby claim the benefit under Title 35, United States Code §120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code §112, I acknowledge the duty to disclose information material to patentability as defined in Title 37, Code of Federal Regulations, §1.56 which occurred between the filing date of the prior application and the national or PCT international filing date of this application:

APPLICATION SERIAL NO.	U.S. FILING DATE	STATUS: PATENTED, PENDING, ABANDONED

And I hereby appoint Michael R. Davis, Reg. No. 25,134; Matthew M. Jacob, Reg. No. 25,154; Warren M. Check, Jr., Reg. No. 33,367; Nils Pedersen, Reg. No. 33,145; Charles R. Watts, Reg. No. 33,142; and Michael S. Huppert, Reg. No. 40,268, who together constitute the firm of WENDEROTH, LIND & PONACK, L.L.P., as well as any other attorneys and agents associated with Customer No. 000513, to prosecute this application and to transact all business in the U.S. Patent and Trademark Office connected therewith.

I hereby authorize the U.S. attorneys and agents named herein to accept and follow instructions from NORSK HYDRO ASA as to any action to be taken in the U.S. Patent and Trademark Office regarding this application without direct communication between the U.S. attorneys and myself. In the event of a change in the persons from whom instructions may be taken, the U.S. attorneys named herein will be so notified by me.

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I further declare that all statements made herein of my own knowledge are true, and that all statements on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code, and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

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The above application may be more particularly identified as follows:

U.S. Application Serial No. 09/857,415 Filing Date June 4, 2001

Applicant Reference Number VHJ:EMH-P9881 Atty Docket No. 2001\_0698A

Title of Invention METHOD FOR RECOVERING CO<sub>2</sub>